

Amendments to the Claims:

This listing of claims will replace all prior versions and listings, of claims in the application:

Listing of Claims:

Claims 1-7 (Cancelled)

8. (Currently Amended) Process for [the] a catalytic fluorination of saturated or olefinic halogenated hydrocarbon(s) ~~hydrocarbons by HF in the gas phase, the method comprising flourination of saturated or olefinic halogenated hydrocarbon(s) by HF in a gas phase and in the presence of [with] a bulk catalyst based on chromium and on nickel which are obtained by impregnation of an amorphous chromium III oxide with a solution of a nickel compound derivative,~~

wherein characterized in that the chromium oxide used exhibits a BET specific surface area of greater than 150 m²/g and a pore volume of greater than 0.15 ml/g;

wherein the catalyst is dried under an inert gas or under air at a temperature of between 100 and 350°C and then activated with HF,

wherein HF is first introduced diluted in air or in an inert gas at a temperature ranging from 150 to 200°C and then with pure HF at a temperature of less than 400°C, and

wherein the Ni/Cr atomic ratio is between 0.02 and 0.4:1.

9. (Canceled).

10. (Canceled).

11. (Previously Presented) Process according to Claim 8, wherein the fluorination temperature is between 50 and 500°C.

12. (Currently Amended) Process according to Claim 8, wherein the ~~contact~~ fluorination time is between 3 and 100 seconds.

13. (Previously Presented) Process according to Claim 8, wherein the molar ratio: HF/halogenated hydrocarbon(s) is between 1/1 and 30/1.

14. (Previously Presented) Process according to Claim 8, wherein the fluorination is carried out at an absolute pressure of between 0.08 and 2 MPa.

15. (Currently Amended) Process according to Claim 8, wherein the fluorination is carried out in the presence of an oxidizing agent[, ~~optionally oxygen or air~~].

16. (Previously Presented) Process according to Claim 8, wherein the catalyst, deactivated by coking, is regenerated by treatment with air or with oxygen or by a Cl₂/HF mixture, at a temperature of between 250 and 400°C.

17. (Previously Presented) Process according to Claim 8, wherein the halogenated hydrocarbon is perchloroethylene or 1-chloro-2,2,2-trifluoroethane.

18. (Currently Amended) Process according to Claim [10] 8, wherein the catalyst is activated with pure HF at the temperature [is] between 350 and 380°C.

19. (Currently Amended) Process according to Claim 11, wherein the fluorination temperature is between 100 and 450°C.

20. (Currently Amended) Process according to Claim 11, wherein the fluorination temperature is between 120 and 400°C.

21. (Currently Amended) Process according to Claim 12, wherein the fluorination contact time is less than 30 seconds.

22. (Currently Amended) Process according to Claim 13, wherein the HF/halogenated hydrocarbon(s) molar ratio is less than 20/1.

23. (Previously Presented) Process according to Claim 14, wherein the pressure is between 0.1 and 1.5MPa.

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24. (New) Process according to Claim 15, where the oxidizing agent is air or oxygen.